

We claim

1. An integrated process for the simultaneous recovery of industrial grade potassium chloride and low sodium edible salt with overall KCl yield of 90-95%, which comprises
 - 5 (i) desulphatation of bittern with a solution of calcium chloride;
 - (ii) subjecting the desulphated bittern to evaporation till density of 32 to 32.5 °Be' (sp.gr.1.283-1.288) is achieved;
 - (iii) mixing the desulphated bittern obtained in step (ii) with a concentrated solution of $MgCl_2$ to obtain high purity carnallite;
 - 10 (iv) decomposing the carnallite with water to obtain ca. 60 % of overall KCl and residual bittern;
 - (v) concentrating residual bittern to obtain residual NaCl and KCl in bittern in the form of crude carnallite and carnallite decomposed liquor;
 - (vi) 15 decomposing the crude carnallite obtained in step (v) with water to produce KCl-enriched low sodium salt in 30-35% overall yield with respect to KCl in the original 32 to 32.5 °Be' (sp.gr.1.283-1.288) bittern, as well as carnallite decomposed liquor;
 - (vii) 20 collecting carnallite decomposed liquor obtained in steps (v) and (vi) above and treating with upgraded lime to generate low boron magnesium hydroxide and filtrate containing $CaCl_2$ and KCl;
 - (viii) 25 recycling the filtrate obtained in step (vii) above to step (i) above for desulphatation of bittern while simultaneously recovering KCl lost in carnallite decomposed liquors;
 - (ix) recycling the $MgCl_2$ -rich end bittern of step (iii) for sustained production of high purity carnallite and also for production of $CaCl_2$, and
 - (x) 30 utilizing any excess $MgCl_2$ to recover bromine and obtain $MgCl_2 \cdot 6H_2O$ and its derivatives.
2. A process as claimed claim 1 wherein in step (i) the density of bittern taken is in the range of 28-30 °Be' (s.g 1.24-1.26).
3. 30 A process as claimed claim 1 wherein in step (i) the stoichiometric ratio of $CaCl_2$ to SO_4^{2-} is in the ratio of 0.9:1 to 1.1:1, and preferably 1:1.
4. A process as claimed claim 1 wherein in step (iv), one part of 32 to 32.5 °Be' (sp.gr. 1.283-1.289) is mixed with 2.0-2.5 parts of end bittern containing 400-440 g/L

- MgCl₂ and the density of the resultant bittern is in the range of 34.0-35.0 °Be' (sp.gr. 1.306-1.318) and more preferably in the range of 34.4-34.6 °Be'. (sp.gr. 1.311-1.315).
5. A process as claimed claim 1 wherein in step (iii) the 32-32.5 °Be' (sp.gr. 1.283-1.289) bittern is filtered if required to remove insoluble matter such as dust, black particles and organic matter.
6. A process as claimed Claim 1 wherein in step (iv), the NaCl content of carnallite is in the range of 0.2-2.0 %, preferably in the range of 0.2-0.4%.
7. A process as claimed claim 1 wherein in step (iv) the purity of KCl obtained is in the range of 97-99 % after washing with water to remove adhering MgCl₂.
10. 8. A process as claimed claim 1 wherein in step (v), the bittern is concentrated to a final density of 36.5-37.2 °Be' (sp.gr. 1.306-1.318) either by solar evaporation or preferably through forced evaporation in an open pan or still more preferably in a multiple effect evaporator for recovery of water.
9. A process as claimed claim 1 wherein in step (v) the crude carnallite contains 14-16% KCl and 18-22% NaCl.
15. 10. A process as claimed claim 1 wherein in step (vi) the low sodium salt contains 40-50% KCl and 50-60% NaCl.
11. A process as claimed claim 1 wherein in step (vii), the carnallite decomposed liquor contains 15-20 mg/L B₂O₃ and 60-80 g/L Mg.
20. 12. A process as claimed claim 1 wherein in step (vii), the Mg(OH)₂ obtained is converted into MgO containing < 0.02 % B₂O₃.
13. A process as claimed claim 1 wherein in step (vii), the filtrate contains 15-30% CaCl₂ and 5-10% KCl.

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